

Improving the flexibility of hard-coal fired power plants by means of APC





1	Introduction
	Introduction

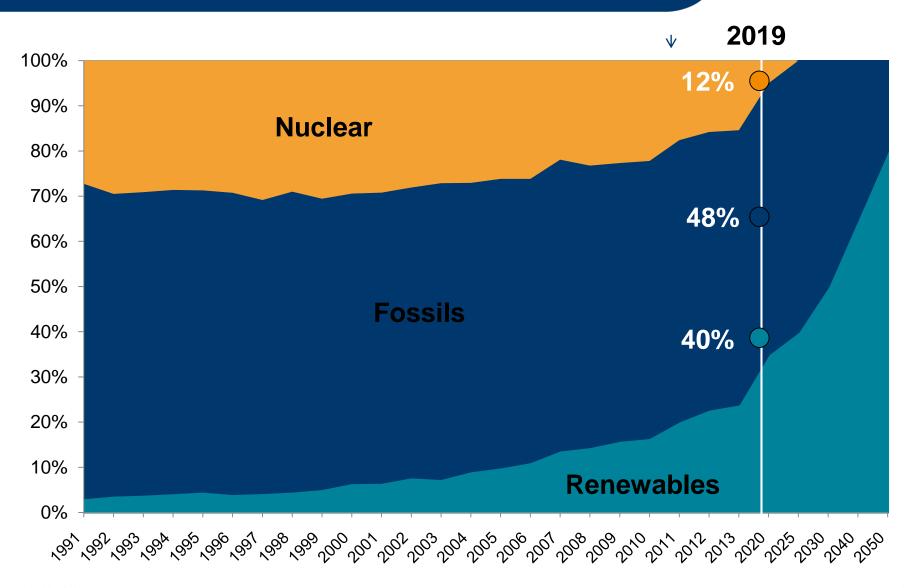
- 2 Minimum load reduction
- 3 Start-up optimization
- 4 Frequency control
- 5 Combustion Optimization
- 6 Summary



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2	Minimum load reduction	
3	Start-up optimization	
4	Frequency control	
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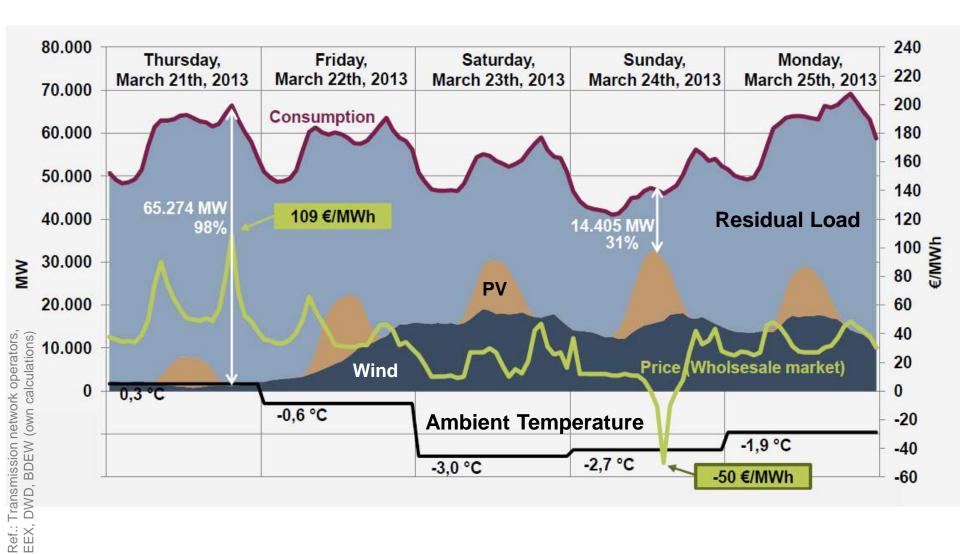
## Development and Outlook of Renewable and Conventional Power Generation in Germany





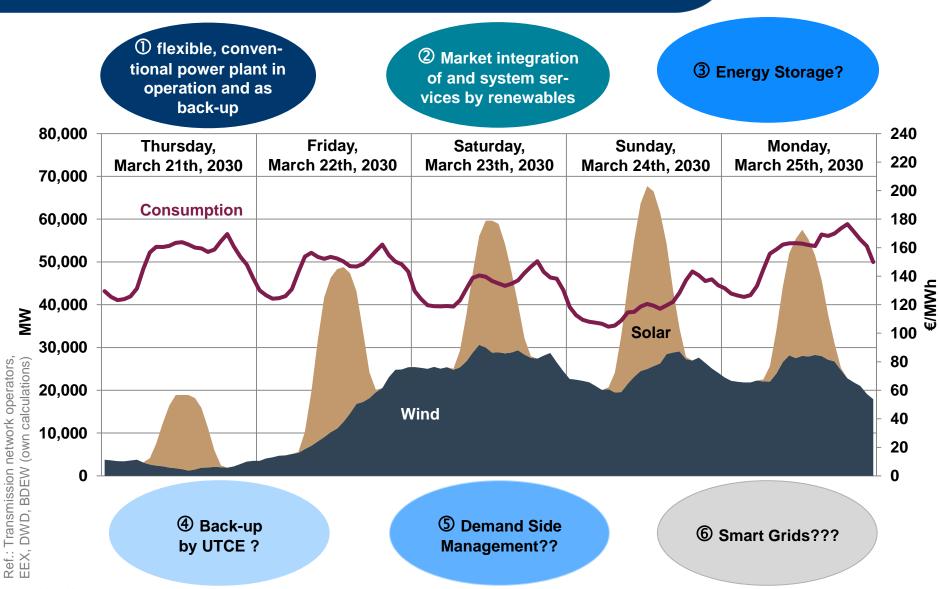
## Renewables and Conventional Power Plants feeding into the German Grid





#### What will be the situation in 2030?



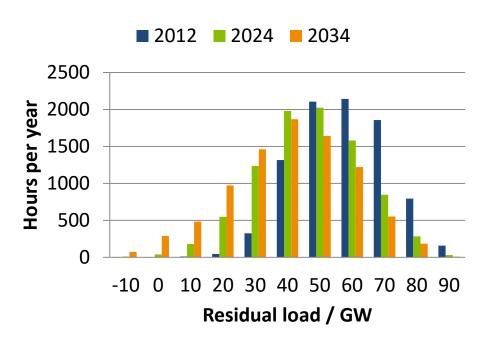


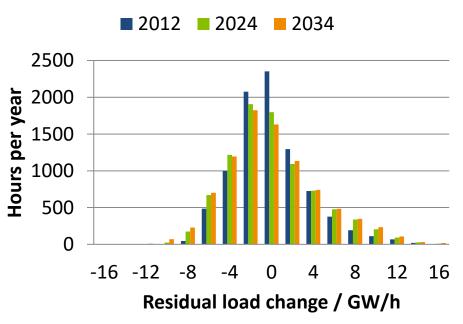
#### **Residual load in Germany**



Dispatchable energy sources cover the residual load

$$P_{\text{Residual}} = P_{\text{Total}} - P_{\text{PV}} - P_{\text{Wind, onshore}} - P_{\text{Wind, offshore}}$$





 Flexible capacity (reduced minimum load and optimized start-up) by thermal power plants are still necessary

## Flexible, conventional power plant in operation and as back-up



- Conventional power plants can be optimized.
- Optimisation done:
  - Reduction of minimum load
  - Optimisation of start-up
  - Optimisation of load-ramps
- Financial situation of power plants is very tight:
  - Low prices on the electricity market
  - Unadequate reimbursement for system services like redispatch etc

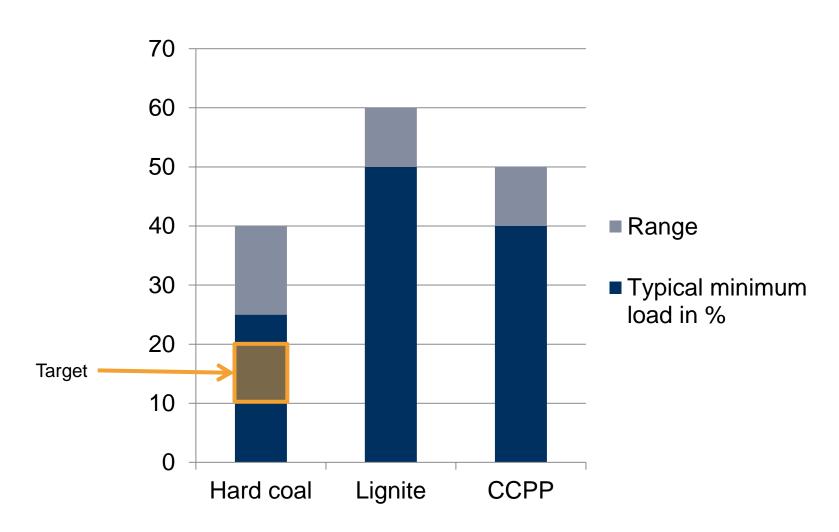




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3	Start-up optimization	
4	Frequency control	
5	Combustion Optimization	
6	Summary	

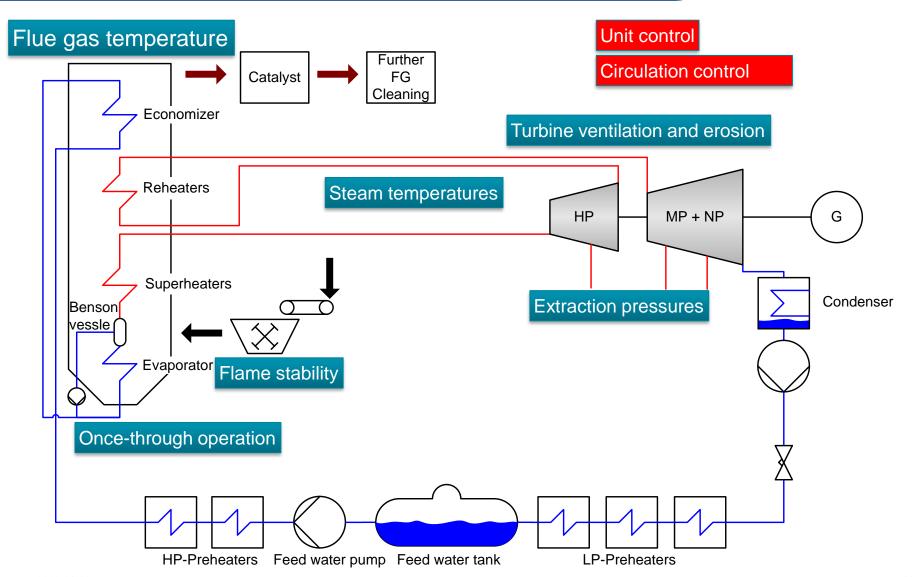
## **Target load**





### Some limiting factors for minimum load

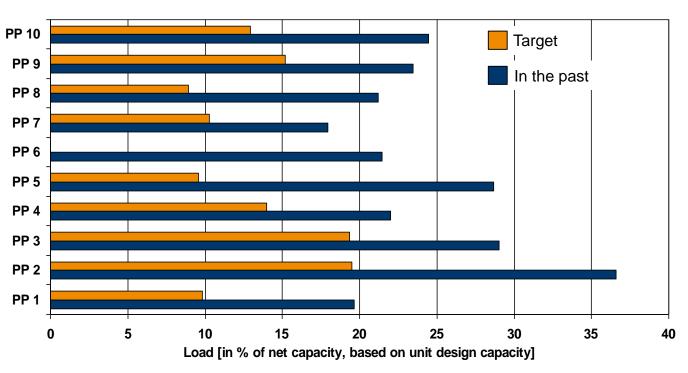




#### **Potential for Minimum Load Reduction**

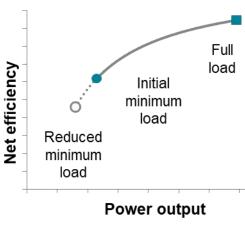


Big potential beyond the initial design



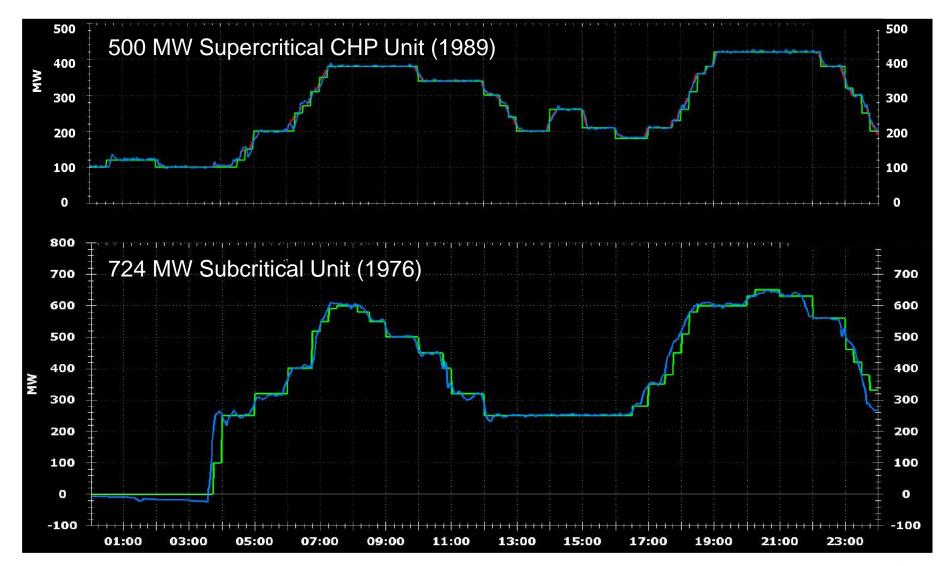


- Reference plants in Germany built between 1970 1990
- But reduction of load will decrease efficiency



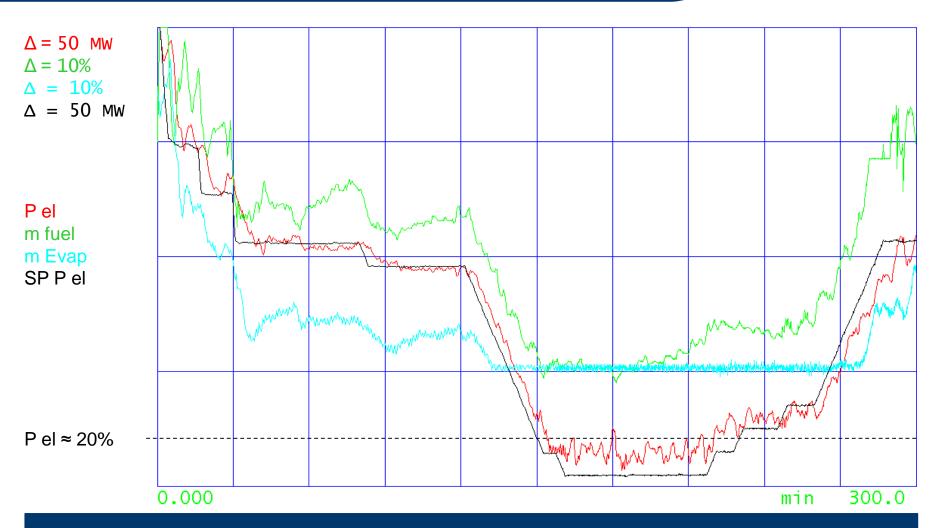
## (2) Optimisation of low load operation of STEAG Power Plants





### **Results in a STEAG power plant**





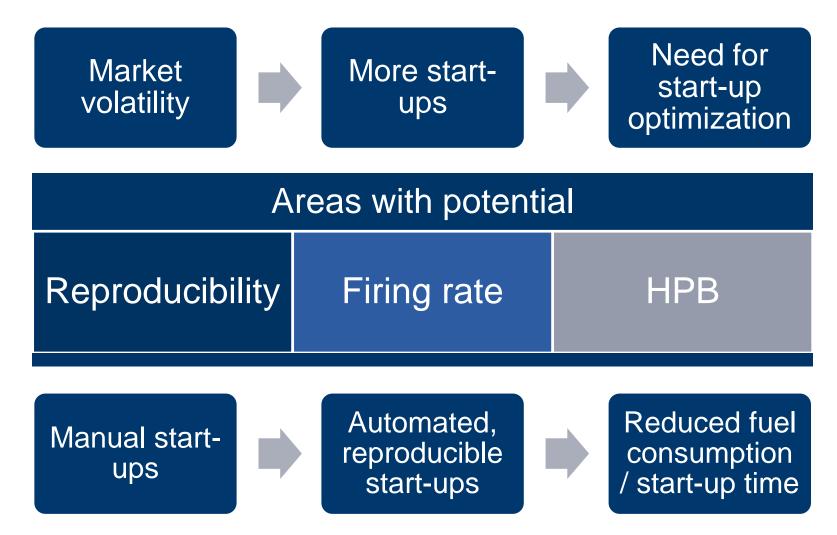
APC based optimization without any process modifications required



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4	Frequency control	
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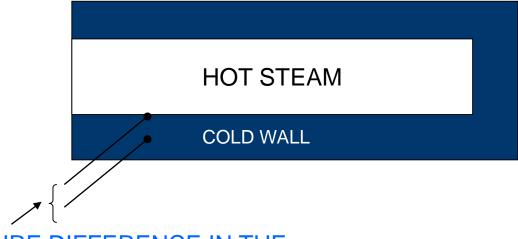
### **Start-up optimization**



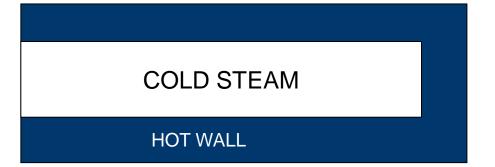


# Thermal Stresses in Header's Wall during Start-Up and Shut Down



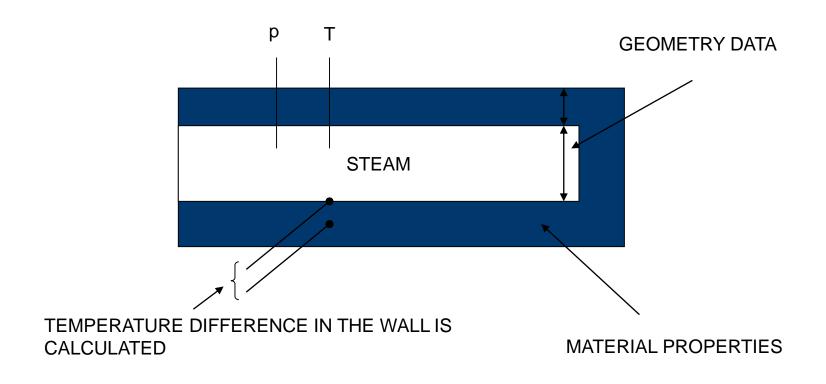


TEMPERATURE DIFFERENCE IN THE WALL OF THE HEADER CAUSES THERMAL STRESS



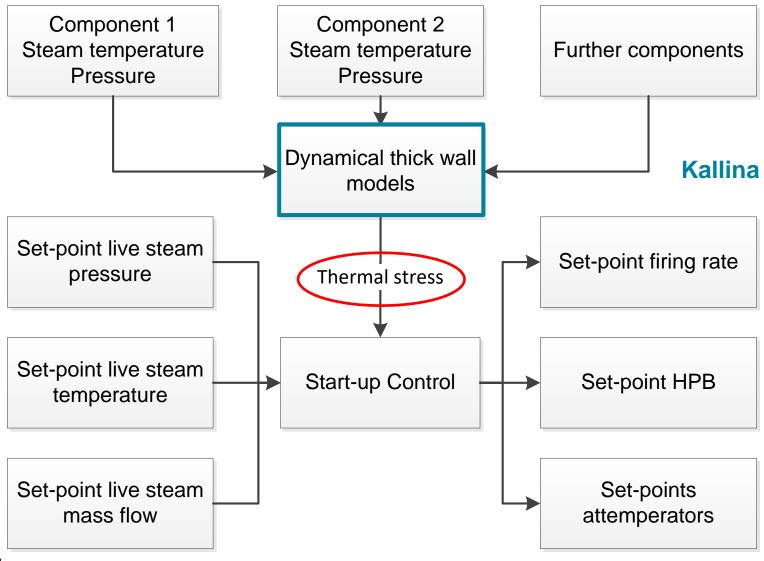
## **Parameter for Calculation of Fatigue**





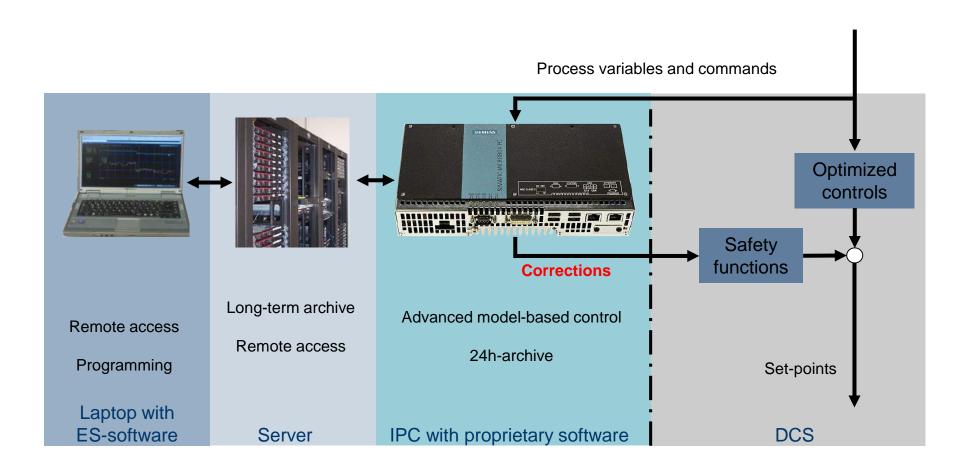
### Start-up control overview scheme





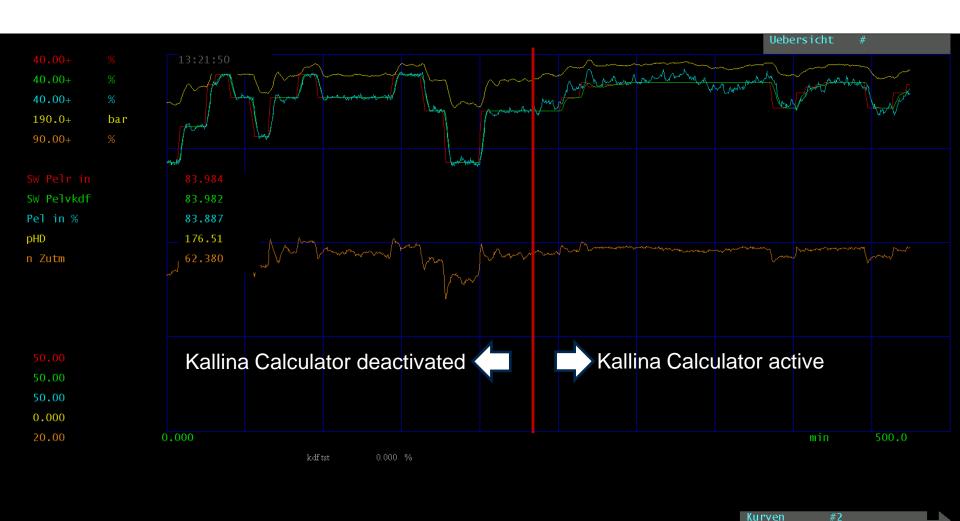
#### **Kallina Calculator**





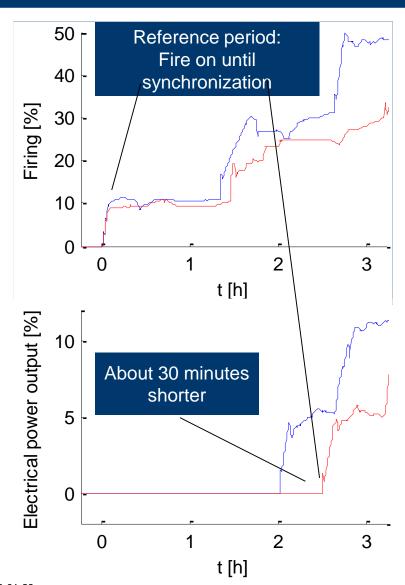
## Kallina Calculator – Optimized vs non-optimized behavior

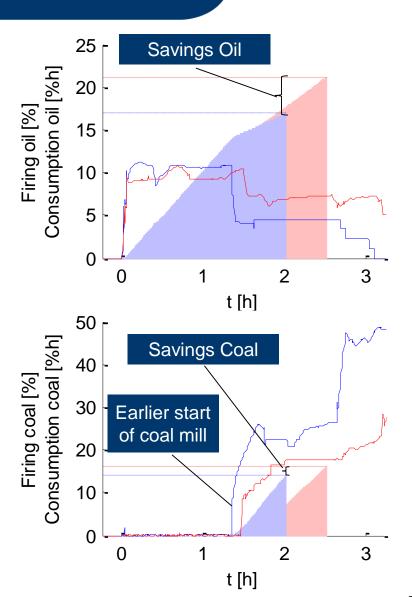




## Results in a STEAG power plant Automated start-up vs. Good manual start-up

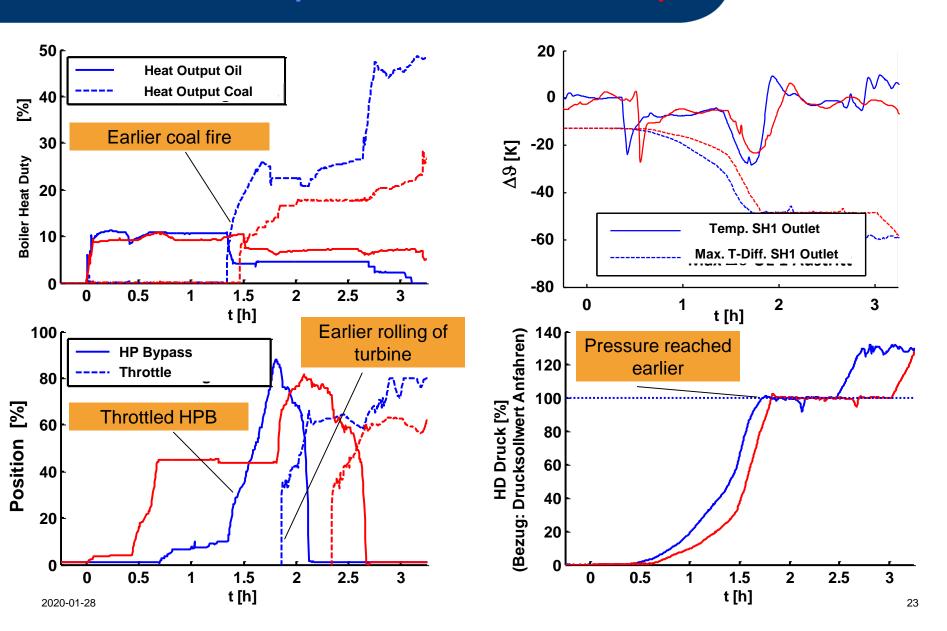






## Results in a STEAG power plant Automated start-up vs. Good manual start-up







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<b>4 5</b>	Frequency control  Combustion Optimization	

#### **Reserve Controls**



#### **Primary control reserve:**

Provided according to the solidarity principle by all Transmission System Operators (TSOs) synchronously connected within the ENTSO-E area Automatic and complete activation of primary control reserve within 30 seconds Period per incident to be covered: 0 < t < 15 min

#### **Secondary control reserve:**

Energy balance of the control area and frequency control immediate automatic activation by the concerned TSO complete activation within five minutes (at most)

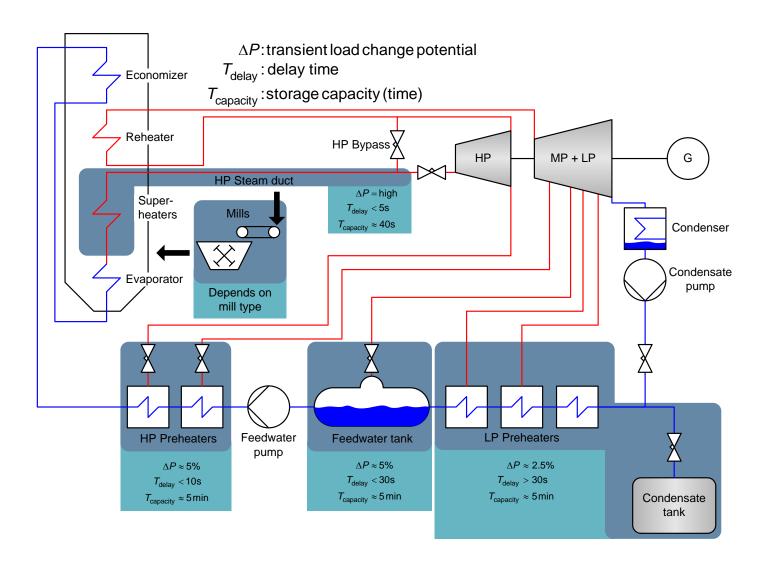
#### **Minute reserve (tertiary control reserve):**

The activation is based on MOLS by a Merit-Order-List (electronical activation) since 2012 Complete activation within fifteen minutes

Period per incident to be covered t > 15 min to 4 quarter hours or up to several hours in case of several incidents

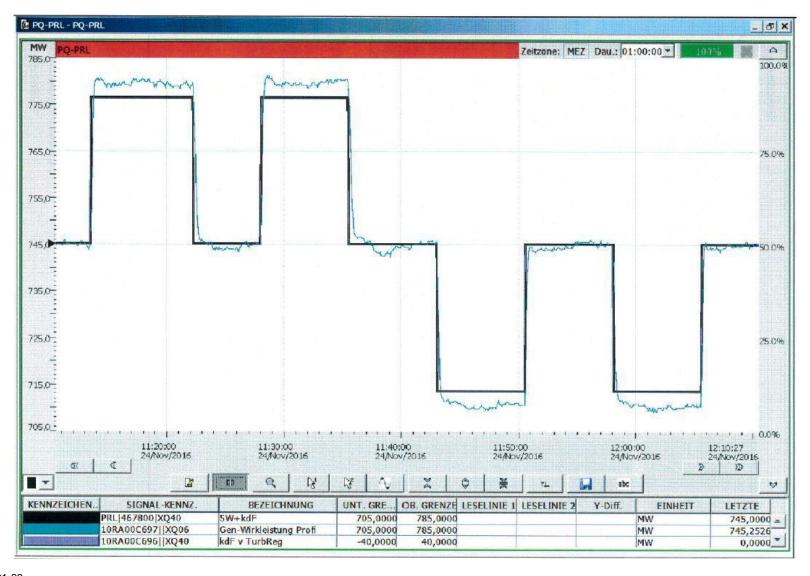
### **Inherent storages**





## Example: 780 MW unit







1	Introduction		
2	Minimum load reduction		
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4	Frequency control		
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## PiT Navigator - APC Solution for Optimization



ANALYSIS O<sub>2</sub>/CO NOx

Targets to be optimized:

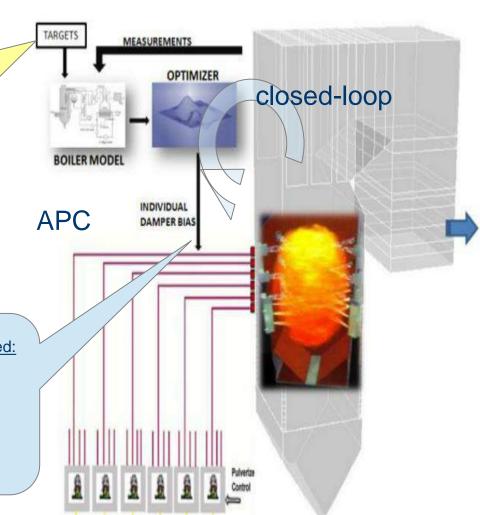
Temperature imbalances

Metal temperatures

Steam temperatures

Efficiency

**NO**x



Outputs (Biases) to be controlled:

Auxiliary air dampers

Cornerwise burner tilts

Over fire air dampers

Mill loading

RH/SH-spray flows

## **Optimization Results from Jharsuguda**



Achieved Improvements	From normal operation	To Pit Navigator	Improvement
Av. duration of RH-Metal Temperature excursion	13min/d	5.9min/d	>50%
Av. RH-Steam Temperature	532.2°C	535.2°C	3K
Av. RH-Spray	49.8t/h	43.9t/h	6t/h
Av. SH-Steam Temperature	538.4°C	539.2°C	0.8K

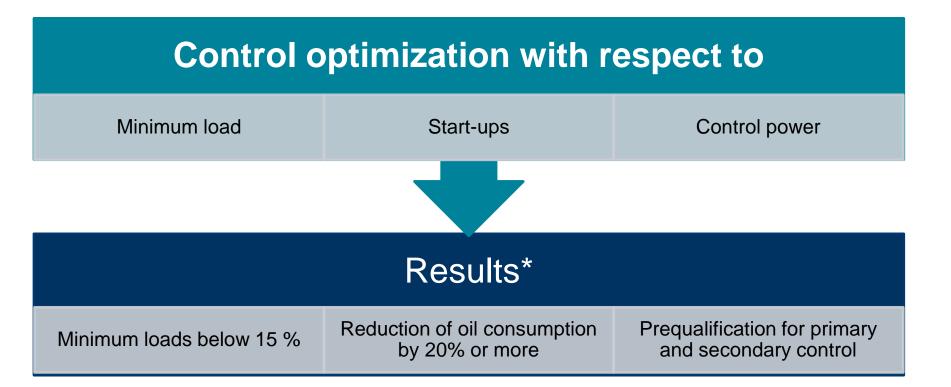
Unit heat rate improvement of 5 kcal/kWh by higher average steam temperatures and reduced RH-spray



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3	Start-up optimization	
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### **Summary**





<sup>\*</sup>general potential; depends on individual plant characteristics

### References



Project	Power Plant Walsum Unit 10/9	Project	Power Plant Zonguldak Unit 2/3
Country	Germany	Country	Turkey
Client	STEAG GmbH	Client	Eren Energji
Technical Data	800 MW / 410 MW – Once through boiler	Technical Data	2*615 MW – Once through boiler
Scope of Services	Minimum load reduction / Frequency control /	Scope of Services	Minimum load reduction – Study
	start-up optimization, soot blowing optimization -	Project Finalization / Duration	2017 / 3 month
	Studies as well as implementation		
Project Finalization / Duration	Since 2010 – ongoing		
Project	Power Plant Bexbach	Project	Power Plant Dadri / Simhadri
Country	Germany	Country	India
Client	STEAG GmbH	Client	NTPC
Technical Data	780 MW – Once through boiler	Technical Data	210 MW / 500 MW – Drum boiler
Scope of Services	Frequency control, ramp rates, SH/RH	Scope of Services	Minimum load reduction / ramp rates / start-up
	Temperature Excursion Reduction – Studies &		optimization – Study
	implementation	Project Finalization/ Duration	2017 / 6 month
Project Finalization / Duration	2016 – 2017		
Project	PPs Guacolda / Bocamina Unit 1/2 / Santa	Project	Power Plant HKW West 2/3
	Maria	Country	Germany
Country	Chile	Client	STEAG GmbH
Client	CDEC SIC	Technical Data	Drum boiler
Technical Data	4*150 MW / 128 MW / 350 MW / 350 MW –	Scope of Services	Ramp Rate Optimization and SH/RH spray optimization
	Drum boiler	Project Finalization / Duration	2012
Scope of Services	Minimum load reduction / ramp rates / start-up	-	
	optimization – Audit		
Project Finalization/ Duration	2015 – 2017		

 ${\sf STEAG\ Energy\ Services-Use\ of\ Advanced\ Process\ Control\ \underline{for}\ Flexible\ Plant\ Operation}$ 

## Thank you very much for your attention!

